



# Performance Impacts of Primary Air



Electric Power 2018

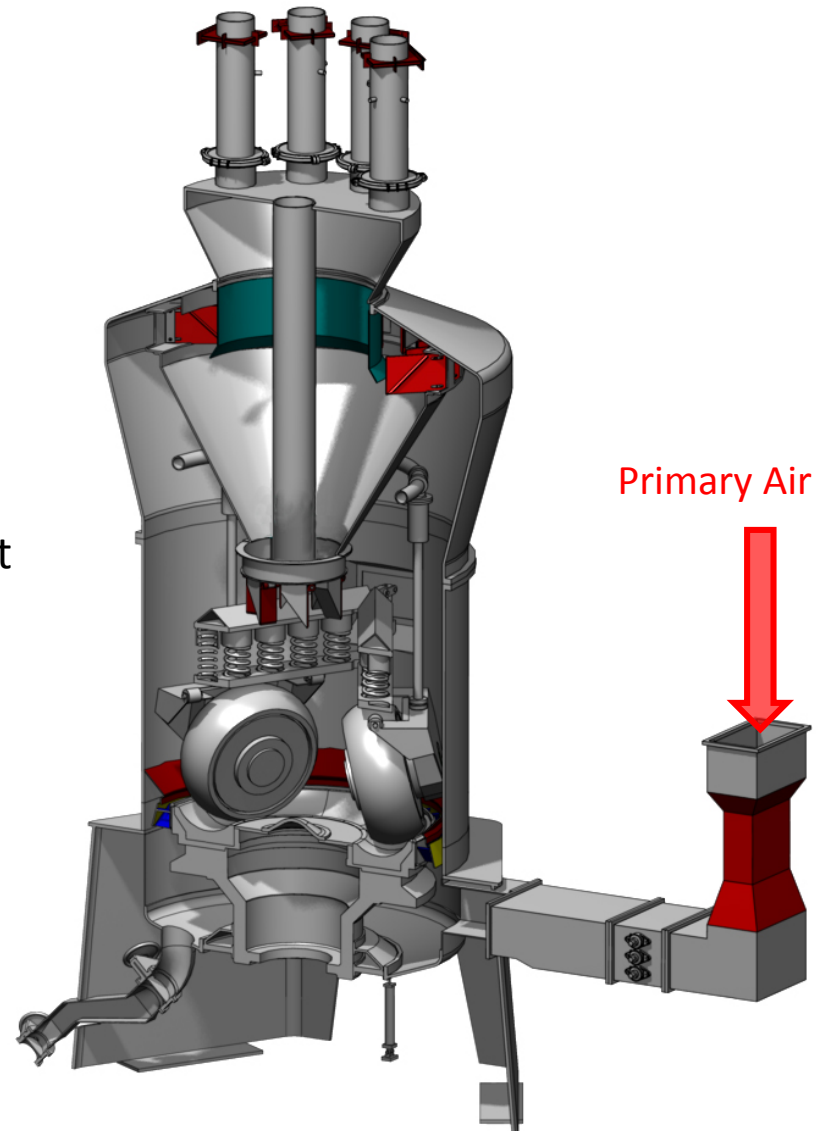
Nashville, TN

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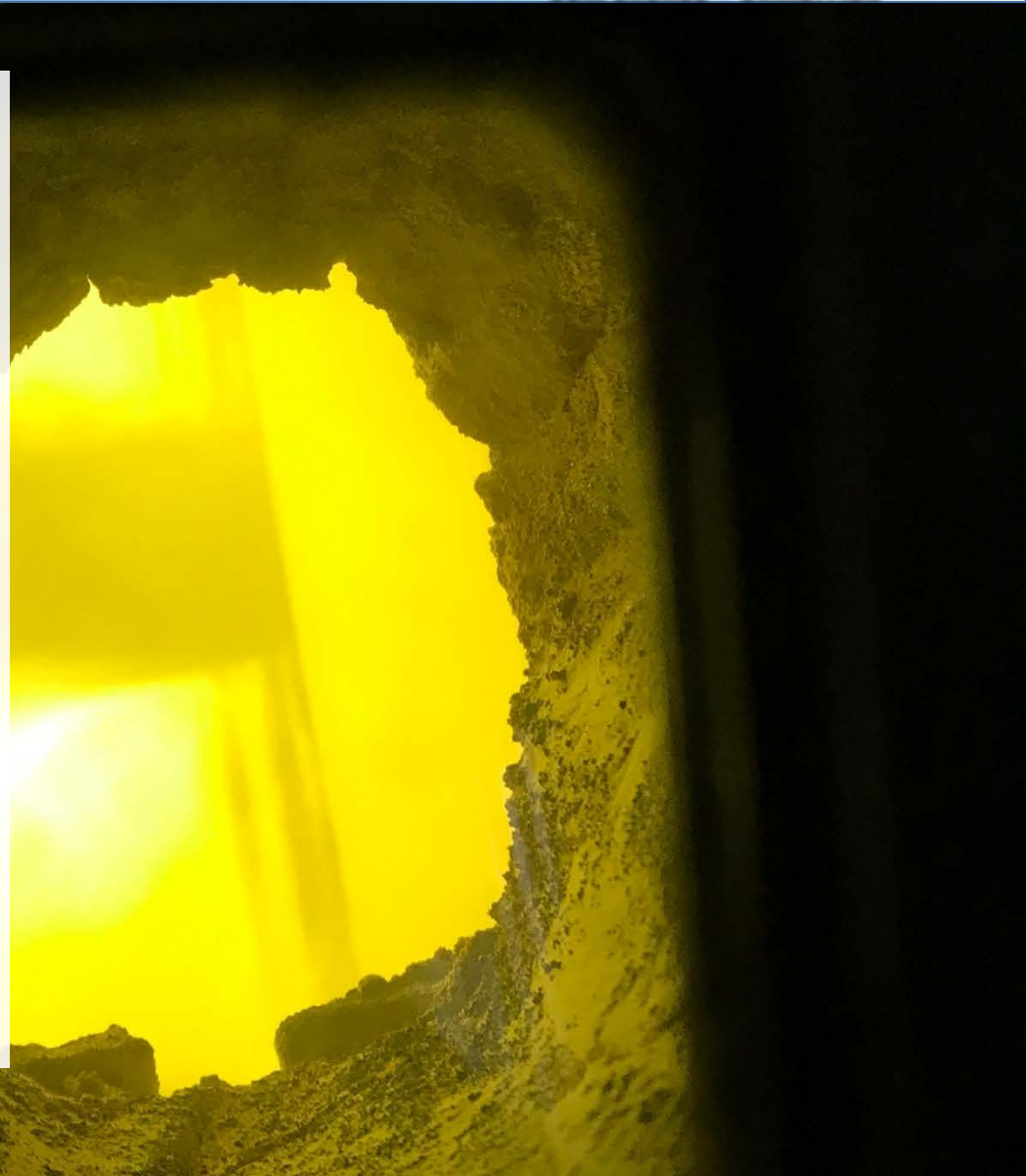


- What is primary air on a pulverized coal boiler?
  - Primary air is air that is heated by the air heater and is used to dry and convey pulverized coal to the boiler
  - 15%-20% of the total air supplied to the boiler is typically primary air
  - Primary air can impact pulverizer performance, reliability, emissions and heat rate



# Primary Air Impacts

- Effects of high primary air
  - Increased NO<sub>x</sub> and CO
  - Increased secondary combustion
  - Increased FEGT's
  - Increased spray flows
  - Increased LOI's
  - Increased slagging
  - Increased erosion
  - Decreased fuel fineness
  - Larger fuel imbalances
  - Detached flames
  - Improved boiler response
  - Decreased heat rate





# Primary Air Impacts

- Effects of too little primary air
  - Increased coal rejects
  - Low fuel line velocities
  - Inability to achieve desired mill outlet temperature
  - Coal layout in the horizontal piping
  - Increased probability of fuel line plugging/fires
  - Increased probability of mill puffs
  - Lack of boiler response



# Primary Air Measurement

- Most common primary air flow measurement devices
  - Pitot tubes
  - Venturis



## Common Low DP Airflow Measurement System Claims:

- Add one pair of sensors per existing duct (air or gas)
  - No calibration
  - No drift
  - No pressure drop
  - No maintenance
- Absolutely linear measurement characteristics
- Installations applicable for all duct dimensions in a wide velocity range
- Easy retrofit into existing ducts
- Not affected by particulate in gas stream



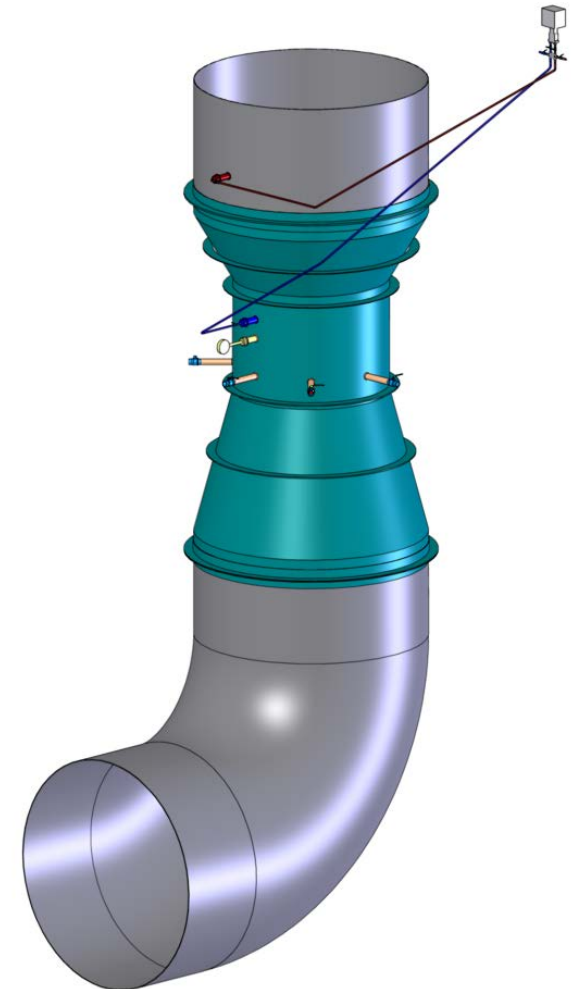
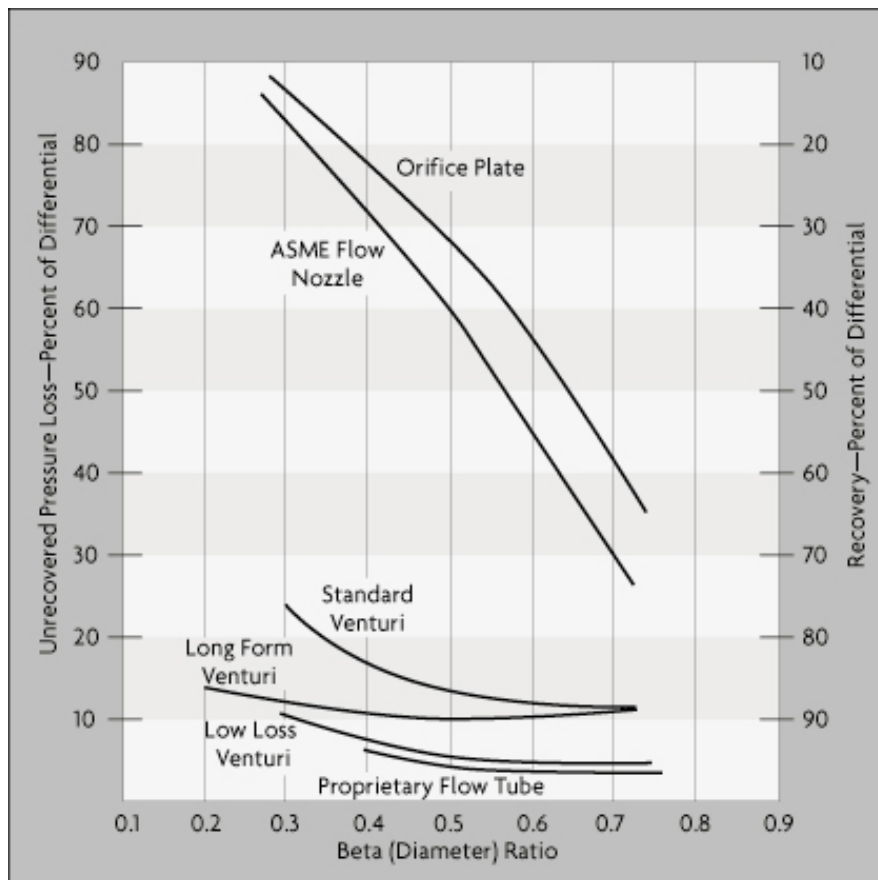
**Storm's experience suggests the need for calibrated and proven flow elements with periodic testing to confirm accuracy**





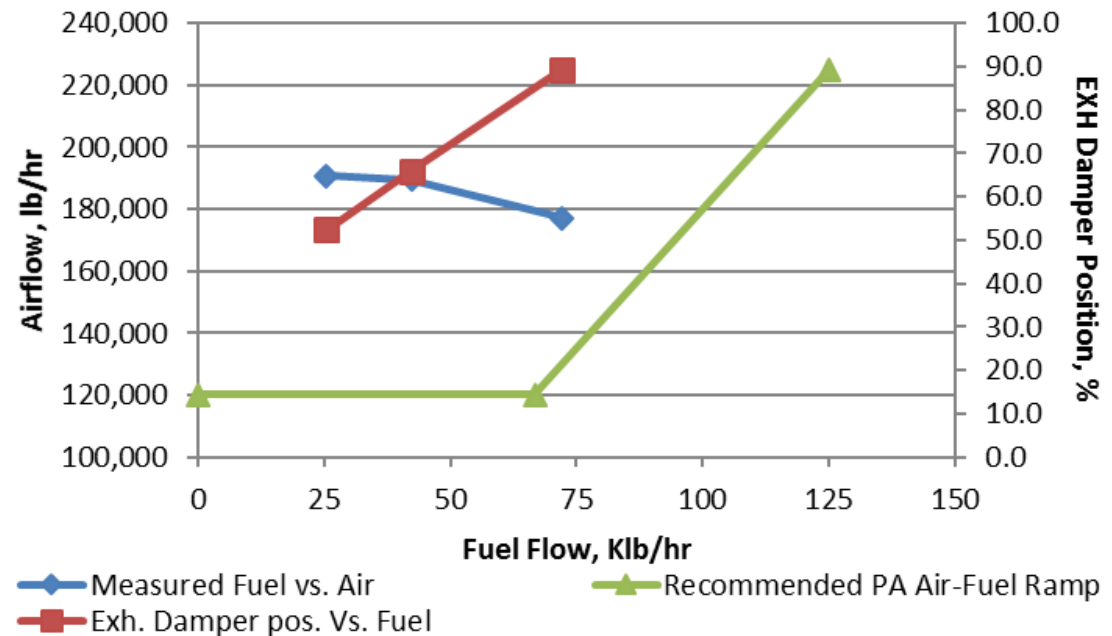
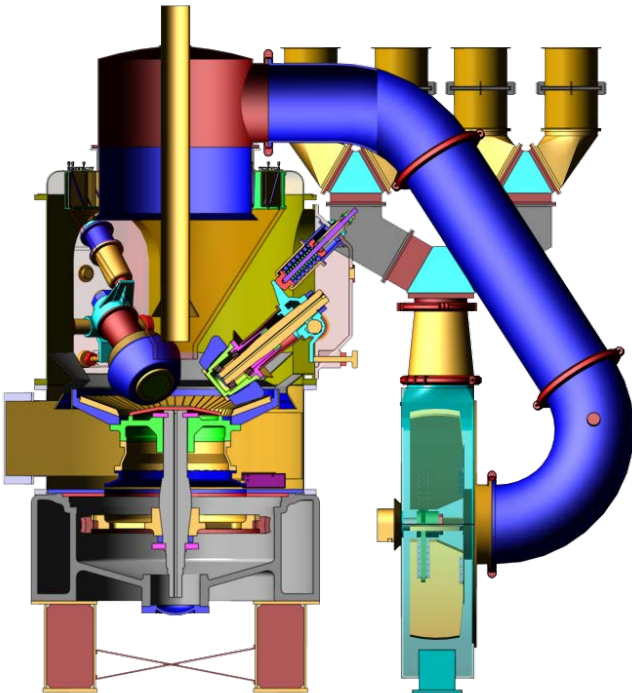
## Common Misconceptions of Venturis

- Too much pressure drop
- Need a long straight run to ensure accuracy



# Measurement and Control

- Most suction mills have no primary air flow measurement
- Exhauster dampers control the suction and primary air to the mill
- Air/fuel ratios are often found extremely outside the recommended range





## Why Hot “K” Calibrations instead of Cold?

Simply, the density of cold air is different from hot air ...

This can lead to a significant variance in given velocity while having a similar mass flow rate. Therefore, when characterizing differential measuring flow elements like Venturis, Pitot tubes or Airfoils, the characterization of the **Differential vs. Flow will change for a given temperature.** Hence, the K-factor will vary. Because of this, we prefer to conduct Hot “K” airflow calibrations that use typical operational air or gas density when developing an average K factor/Curve

### Example #1 (Cold Air)

$$T = 50^{\circ}\text{F}; S_p = 50^{\circ}\text{W.C.}; B_p = 29.5^{\circ}\text{Hg}$$

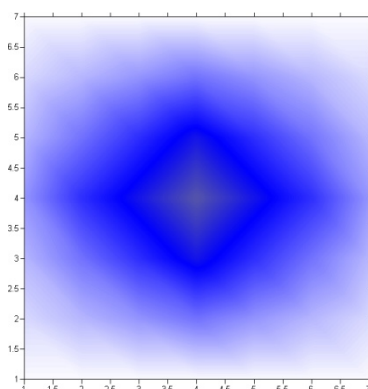
$$\delta = \frac{460 + 70^{\circ}\text{F}}{460 + T} * \frac{B_p + \frac{S_p}{13.6}}{29.92^{\circ}\text{Hg}} * .075 \frac{\text{lbs}}{\text{ft}^3}$$

$$\delta = .0864 \frac{\text{lbs}}{\text{ft}^3}$$

$$W = 100,000 \frac{\text{lbs}}{\text{hr}}; A = 5\text{ft}^2; \delta = .0864 \frac{\text{lbs}}{\text{ft}^3}$$

$$V \left( \frac{\text{ft}}{\text{min}} \right) = \frac{W}{A * 60 \frac{\text{min}}{\text{hr}} * \delta}$$

$$V = 3858 \frac{\text{ft}}{\text{min}}$$



### Example #2 (Hot Air)

$$T = 600^{\circ}\text{F}; S_p = 50^{\circ}\text{W.C.}; B_p = 29.5^{\circ}\text{Hg}$$

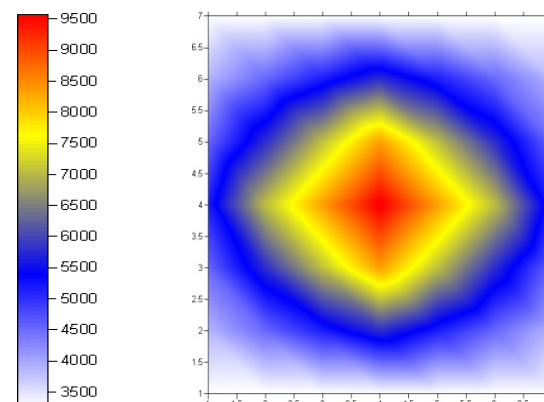
$$\delta = \frac{460 + 70^{\circ}\text{F}}{460 + T} * \frac{B_p + \frac{S_p}{13.6}}{29.92^{\circ}\text{Hg}} * .075 \frac{\text{lbs}}{\text{ft}^3}$$

$$\delta = .029 \frac{\text{lbs}}{\text{ft}^3}$$

$$W = 100,000 \frac{\text{lbs}}{\text{hr}}; A = 5\text{ft}^2; \delta = .029 \frac{\text{lbs}}{\text{ft}^3}$$

$$V \left( \frac{\text{ft}}{\text{min}} \right) = \frac{W}{A * 60 \frac{\text{min}}{\text{hr}} * \delta}$$

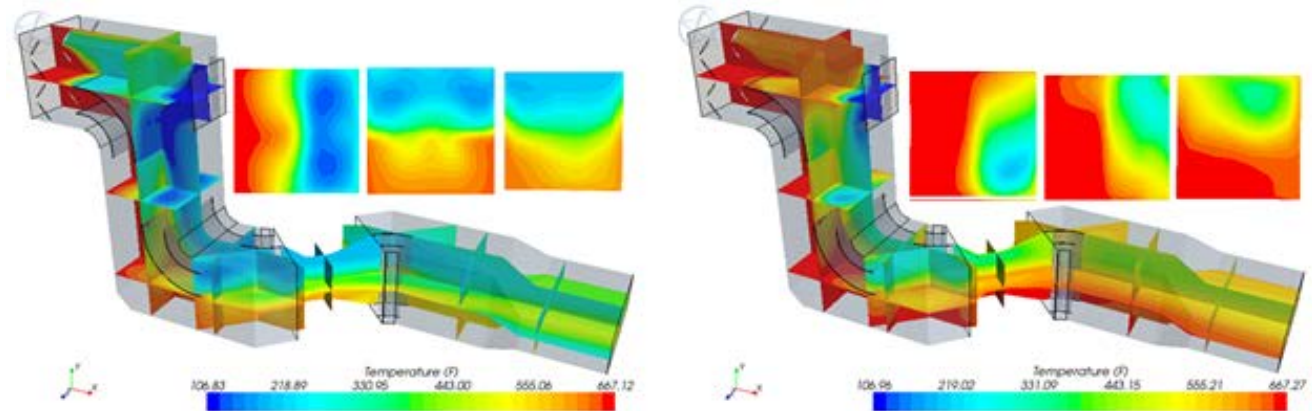
$$V = 11,494 \frac{\text{ft}}{\text{min}}$$



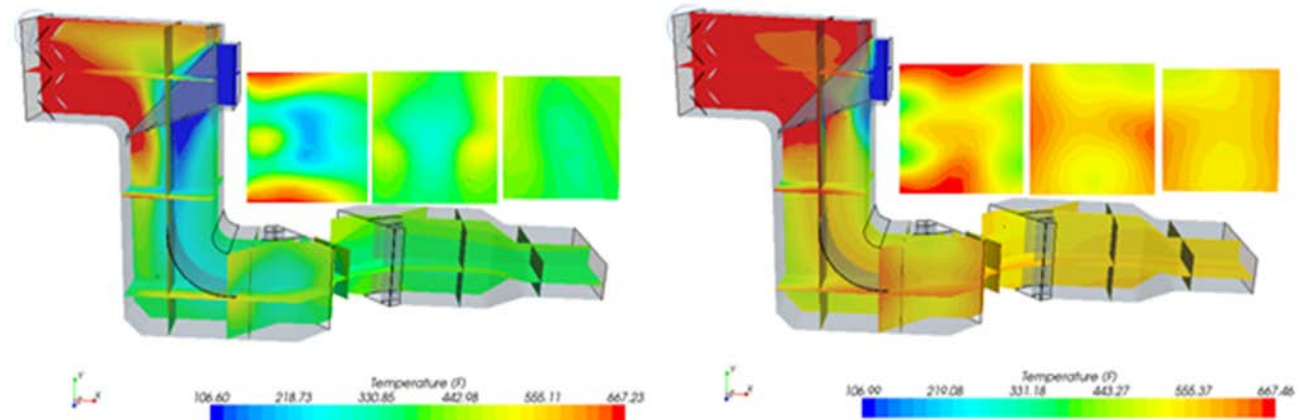
## The importance of Hot “K” Calibrations instead of Cold

- Cold “K” calibrations in this case provided repeatable results where as hot testing did not due to major stratifications in temperature
- Normal operation of the mills without hot “K” calibration testing could have been a safety & reliability hazard

**Pre Mixing Plates**



**Post Mixing Plates**



# Optimizing Primary Air

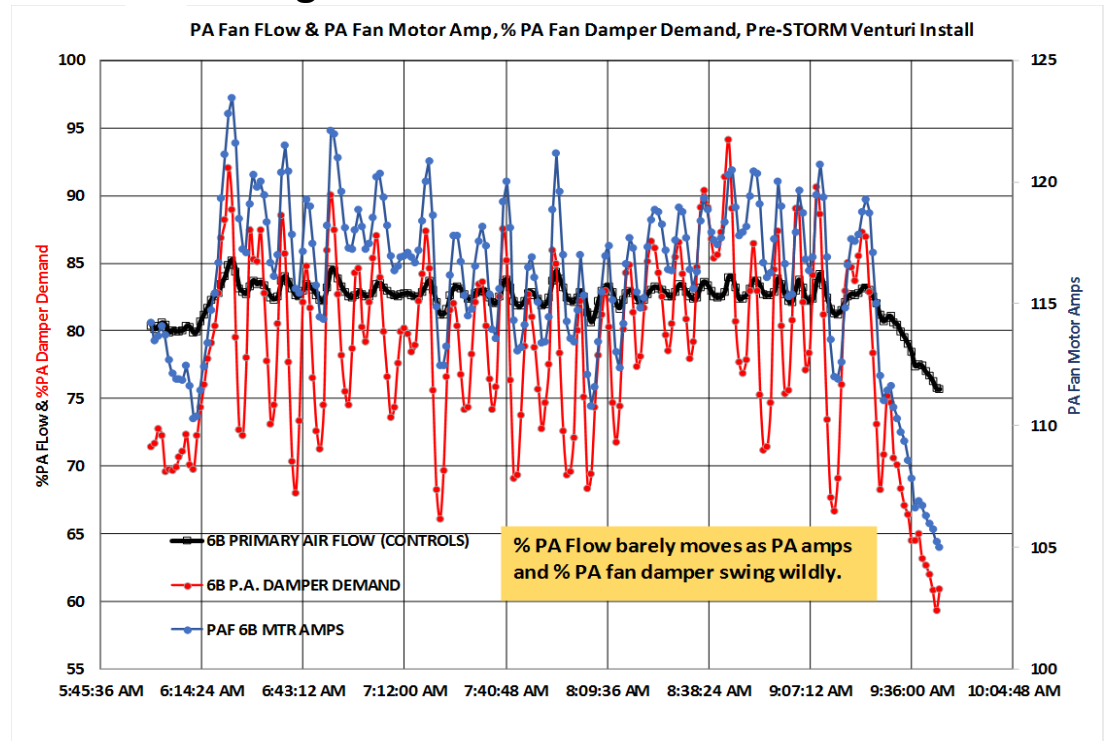
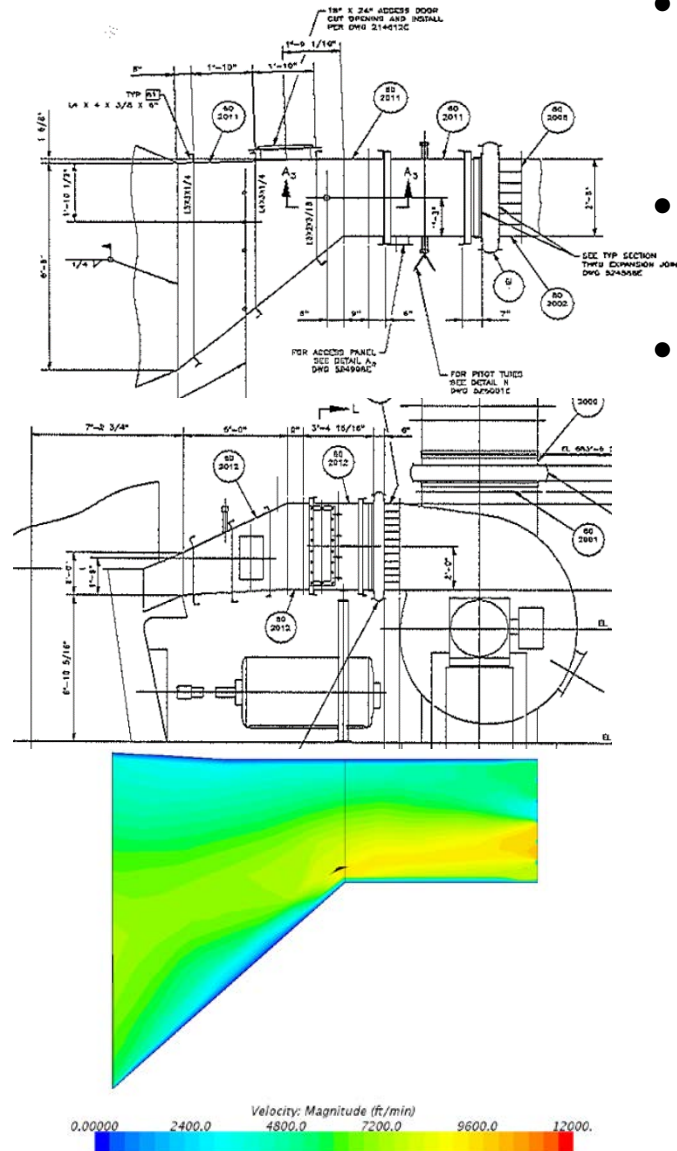
- Primary air flow should be accurately measured and controlled to within  $\pm 3\%$  of the field measured value
- Primary air flow should operate on the recommended air/fuel ramp when above minimum airflow
- Minimum airflow in the fuel lines should be set to allow for no less than 3,300 ft/min velocities
- Hot “K” calibration testing should be completed on an annual basis



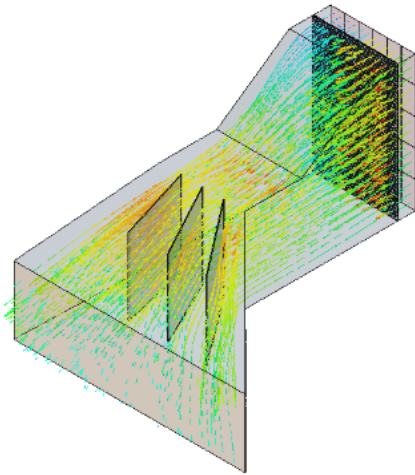


# Field Proven Results: Case #1

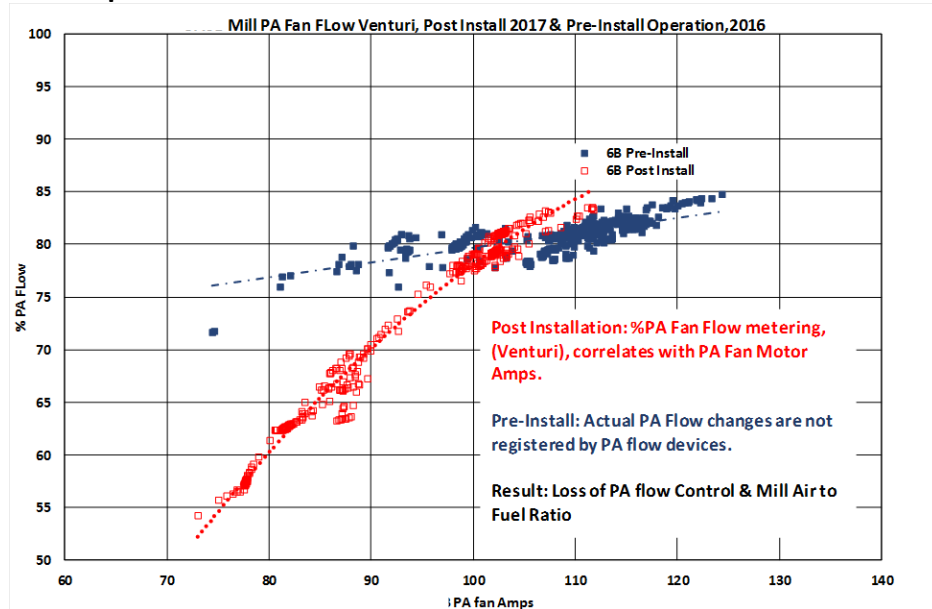
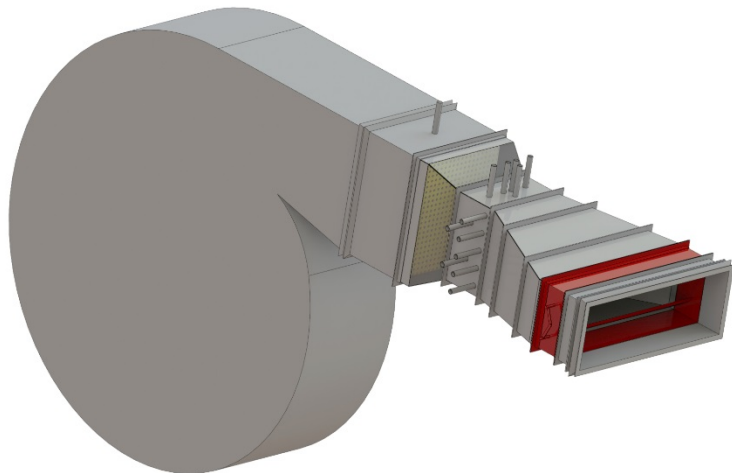
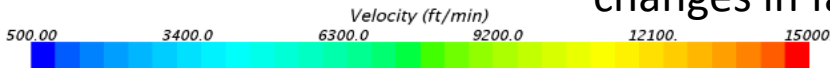
- Poor primary air measurement and control plagued the plant with throttle pressure swings, fuel line fires and poor pulverizer performance
- Pitot tube array located at the discharge of the PA fan did not accurately measure flow.
- PA fan amps and damper changes resulted in nearly no indicated change in PA flow



# Field Proven Results: Case #1

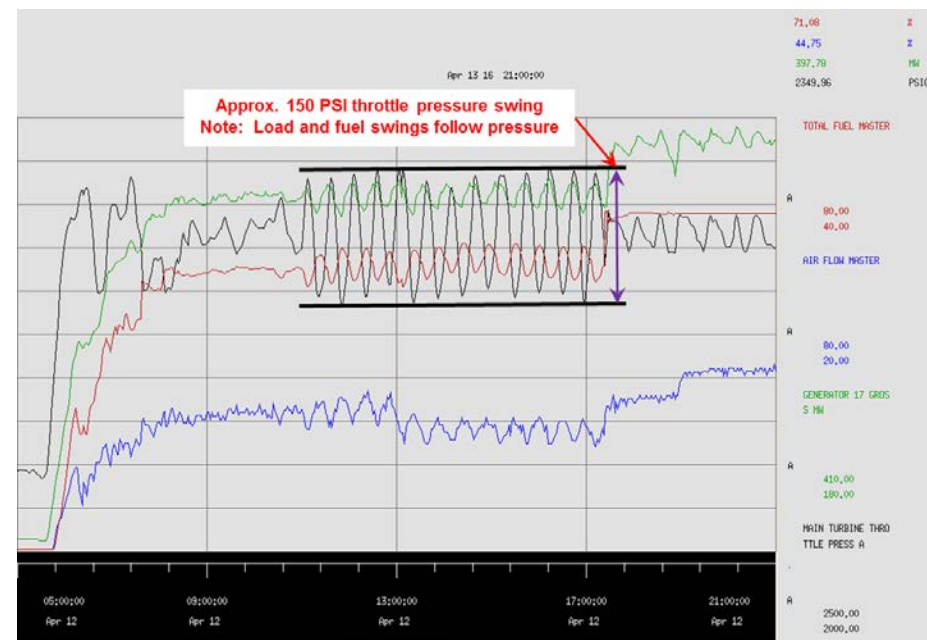


- CFD modeling was utilized in conjunction with field measurements across the full load range of the pulverizer to design a primary air venturi.
- Perforated plate and turning vanes installed to provide more uniform distribution of air through the venturi and at the mill inlet.
- Post installation: PA flow is much more responsive (red) to changes in fan amps



# Field Proven Results: Case #2

- The boiler had historically been unable to operate in AGC due to large throttle pressure swings
- Field testing on the RS 803 pulverizers in 2013 found unresponsive primary air flow with respect to changes in feeder speed
- Unresponsive pulverizers = unresponsive load changes and boiler stability

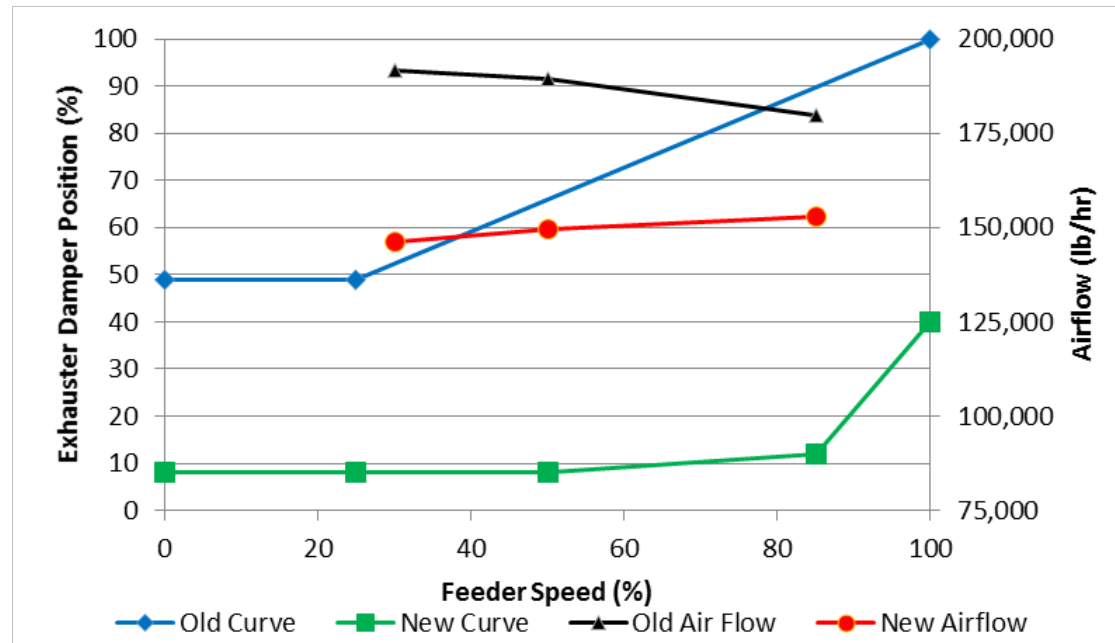
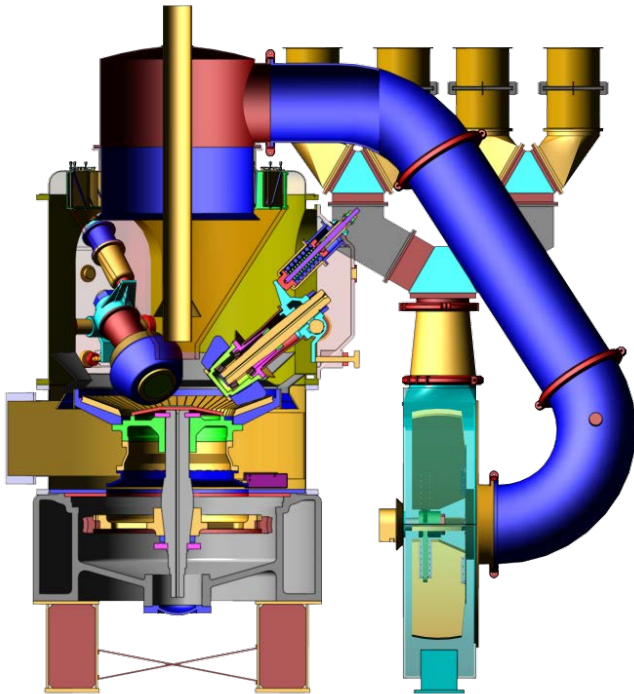


***Note: Each pulverizer responded different and varied some were as much as 12-15 minutes to achieve pressure.***



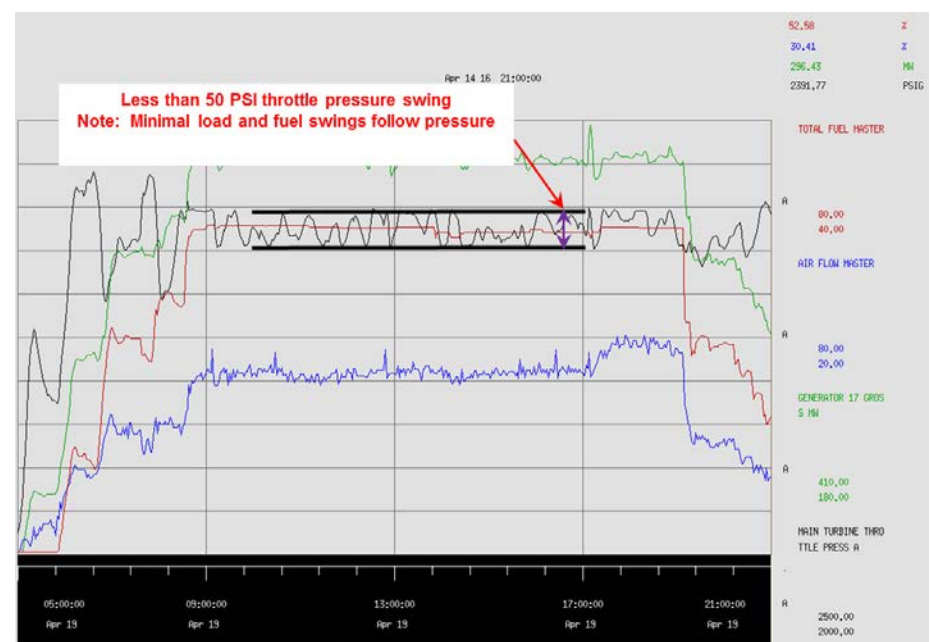
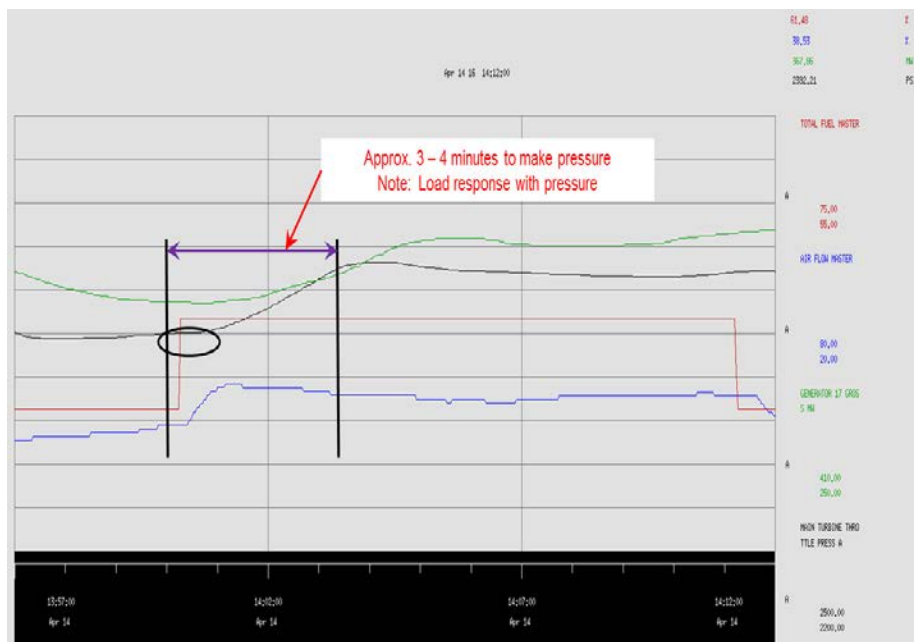
# Field Proven Results: Case #2

- Recharacterizing the exhauster vs. feeder curves for each pulverizer improved boiler stability
- Each pulverizer was tested and exhauster curves varied from mill to mill
- Unit is able to operate in AGC following improved primary air flow control
- Airflow kickers were installed in the control logic to open exhauster damper momentarily during load changes

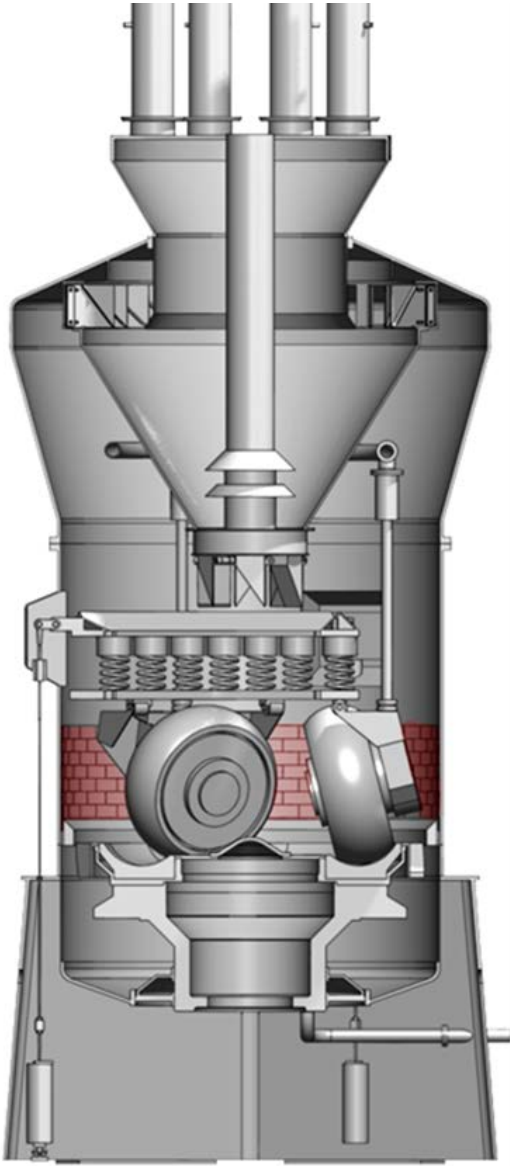


# Field Proven Results: Case #2

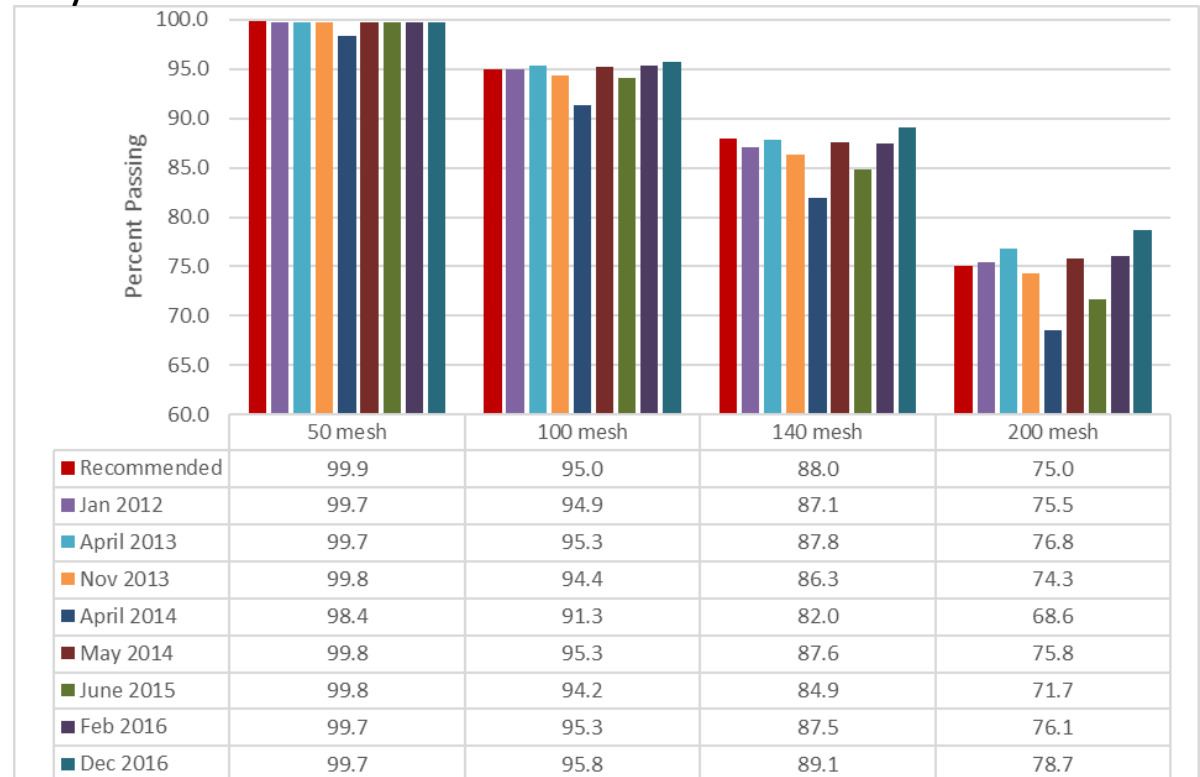
- Recharacterizing the exhauster vs. feeder curves for each pulverizer improved boiler stability
- **Remember each pulverizer was tested and exhauster curves varied from mill to mill**
- Unit is able to operate in AGC following improved primary air flow control



# Field Proven Results: Case #3



- Pulverizer performance has been monitored at the facility consistently since 2008
- Primary air flow is accurately measured, controlled and field checked on an annual basis
- Mill outlet temperatures were operating around 128 deg. F in early 2016

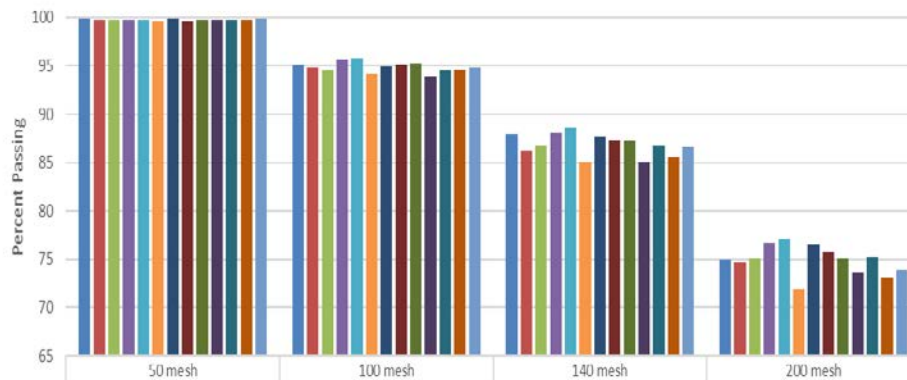




# Field Proven Results: Case #3

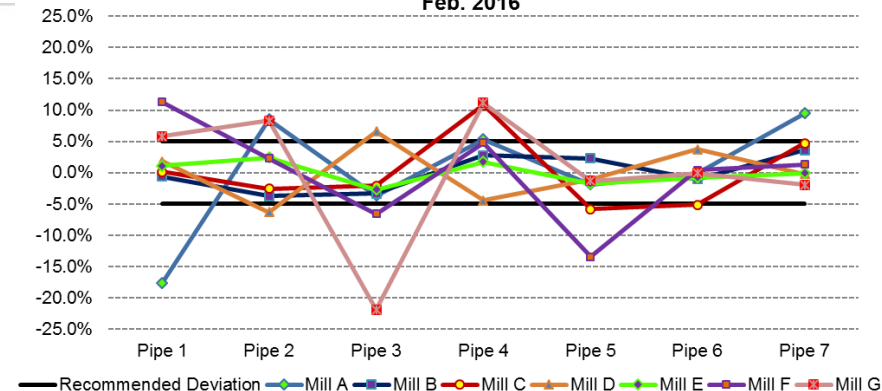
- Lower than desired mill outlet temperatures impact performance by
  - Utilizing higher amounts of tempering air (stealth heat rate penalty)
  - Negatively impacting pulverizer fineness
  - Increased fuel moisture required to be evaporated in the boiler

Fineness Comparison

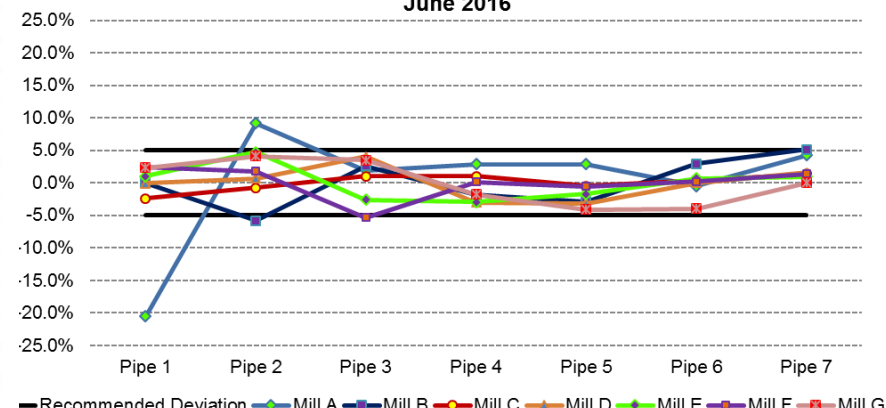


	50 mesh	100 mesh	140 mesh	200 mesh
Recommended	99.9	95	88	75
Mill A @ 128°F	99.8	94.8	86.3	74.7
Mill A @ 135°F	99.7	94.5	86.8	75.1
Mill B @ 128°F	99.8	95.7	88.0	76.7
Mill B @ 135°F	99.8	95.8	88.6	77.2
Mill C @ 128°F	99.7	94.2	85.1	71.8
Mill C @ 135°F	99.9	95.0	87.6	76.5
Mill D @ 128°F	99.7	95.2	87.3	75.7
Mill D @ 135°F	99.8	95.2	87.3	75.1
Mill E @ 128°F	99.8	93.9	85.1	73.6
Mill E @ 135°F	99.8	94.4	86.8	75.1
Mill F @ 128°F	99.7	94.6	85.6	73.0
Mill F @ 135°F	99.9	94.8	86.7	73.9

Fuel Line Air Balance  
Feb. 2016

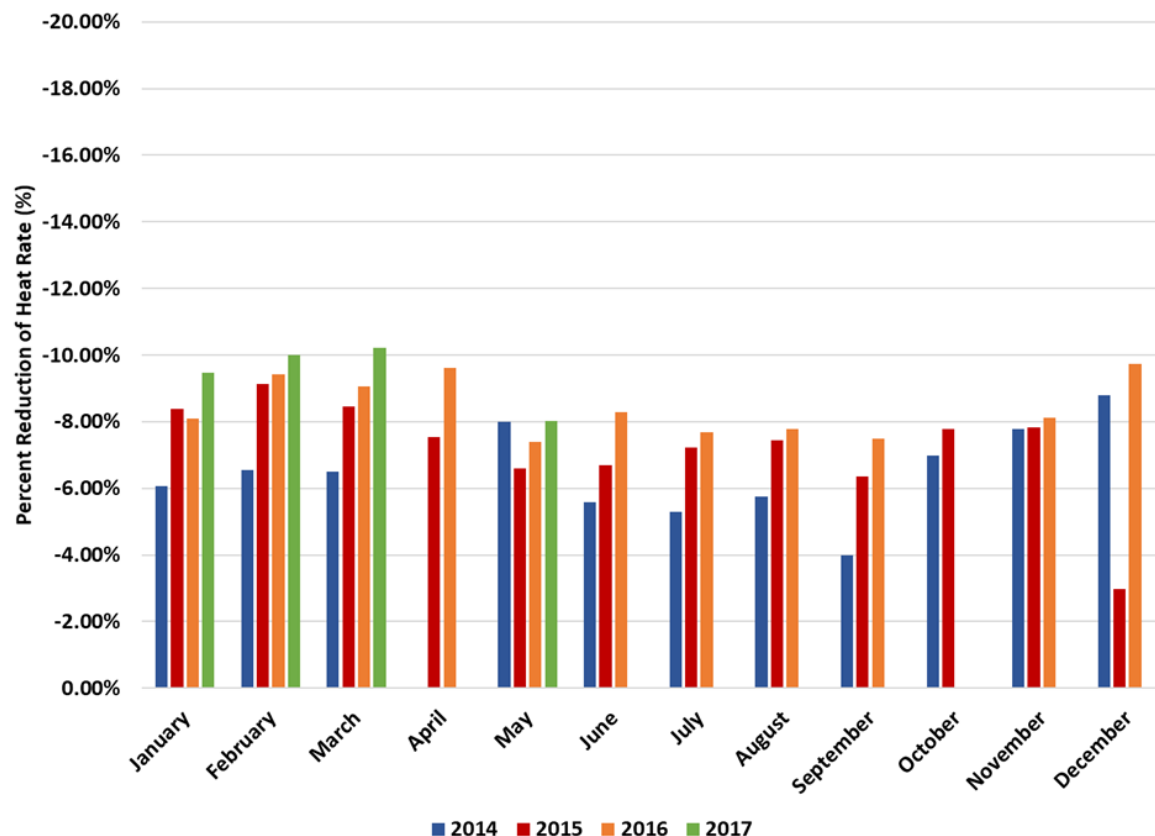


Fuel Line Air Balance  
June 2016



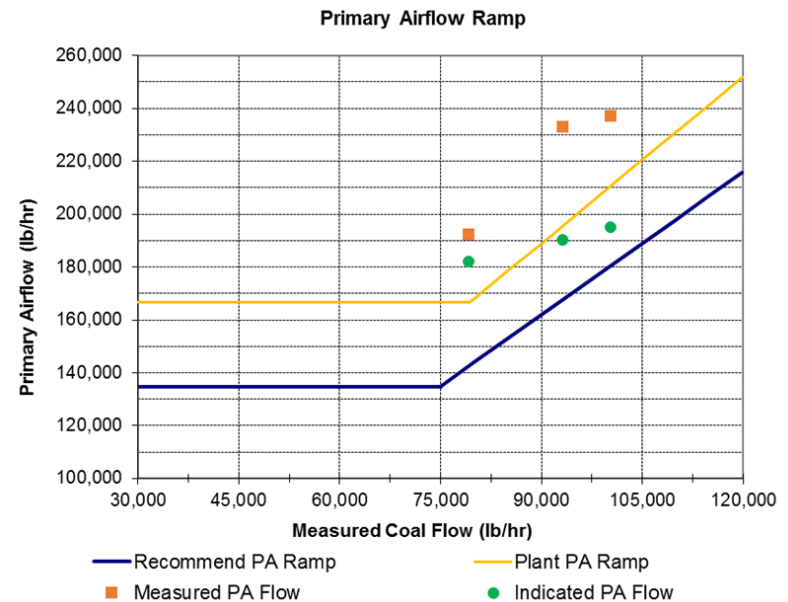
# Field Proven Results: Case #3

- Lower than desired mill outlet temperatures impact performance by
  - Utilizing higher amounts of tempering air (stealth heat rate penalty)
  - On average over 100 Btu/kWhr improvement in heat rate seen following increase in mill outlet temperature set point.



# Final Conclusions

- Roughly 1/5 of the total air to the boiler is primary air, but precise measurement and control of this small percentage is extremely important.
- Primary air can affect boiler response, pulverizer performance, reliability and heat rate
- Minimum primary airflow should be reviewed thoroughly to ensure fuel line and throat velocities are adequate
- Hot “K” calibrations should be completed on at least an annual basis
- Primary air flow should be accurately measured and controlled to within  $\pm 3\%$ .





# Thank You



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